

INDUSTRIAL FILTRATION SYSTEMS

MODEL # GRS-0250-B-CC

OPERATION AND MAINTENANCE MANUAL





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Section 1: Introduction

1.1 Introduction

This following technical manual provides instruction on installation and operation of the Garnet Removal System manufactured by Ebbco Inc. With correct maintenance and system operation the Garnet Removal System will keep garnet form building up in the waterjet cutting machines work tank and will increasing production by eliminating down time for tank shoveling. The Garnet Removal System will require some assembly on site. This will include sweeper package assembly and connecting the Garnet Removal System to the waterjet cutting machines work tank. The Garnet Removal System is manufactured using quality materials and by highly experience production staff. The Garnet Removal System is tested in Ebbco's test department to ensure that it meets the specifications required by the customer. The Garnet Removal System is inspected and all test data documented prior to shipment.

1.2 Sequence of operation.

This system is designed to keep garnet from building up in the cutting table. The method used to achieve this is the use of agitation on the bottom of the tank by water pumped through eductor header nozzles located and directed in engineered locations. The garnet thus stays in suspension due to the agitation and is carried out of the tank by way of the heavy duty centrifugal pump. It is pumped through a centrifugal separator, which concentrates the garnet in the fluid stream and separates it for disposal into an abrasive bag hopper. Excess water that comes out of the separator when it purges the solids from the collection chamber is decanted from the hopper, returning to system tank.



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Section 2: System Specifications

2.1 System utilities requirements

Inlet connection : Outlet connection: Electrical: Full load amps: 3" steel hose barb 2 1/2" steel hose barb 230vac/3ph/60Hz 33.0 amps

2.2 System components

Pump suction basket - PKG-98

Cast iron housing with flanged inlet and outlet connections. Internal basket is constructed of perforated stainless steel.

System pump – PCL 2x3x10B-CC+6

Close-coupled, all iron construction, 316 stainless steel shaft sleeve, semi-open impeller.

Motor: Electrical: Horse power: Full load amp @ 230vac: Speed: Enclosure: Pump: Impeller:

230vac/3ph/60Hz 10 hp 25.6 amps 1760 rpm TEFC PCL 3x4-10-B-CC+6 10"dia.

Centrifugal Separator - SDS-250-B

Carbon steel construction, designed to remove 98% of particulate from liquid, sized at 74 micron and larger with a specific gravity of 2.6 or higher.

Maximum particle size:	3/8-inch
Maximum pressure rating:	150 psi
Pressure loss range:	4.5 to 12 psi

Electrical controller – EHOA-3

Disconnect supplied by others. Provide maximum upstream protection per NEC code 430-52 and table 430-152

Enclosure: Transformer: Filter pump starter module:

Filter pump starter module: PKZ2

Thermal overload yellow dial set point 230vac: Sort circuit red dial set point 230vac:

Pressure gauge – GRS-60-GA Range: Face dia: Inlet size: Case material: Wetted parts: Steel, Nema 12 75va primary/secondary fused Internal sort circuit / thermal overload.

Internal sort circuit / Thermal overload. 25.6 (FLA of motor) 332.8 (13 times FLA of motor)

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0-60 psi 2"

1/4" NPT Stainless/steel Brass

Section 2: System Specifications

Vacuum gauge – GRS-V-GA Range: Face dia: Inlet size: Case material: Wetted parts:

-30inhg - 0 psi 2" 1/4" NPT Stainless steel Brass

Abrasive bag hopper – 1-CUYD-ABH

All carbon steel construction. 1 cubic yard capacity. 3" coupler on decant outlet.

Section 3: System Installation and Start-Up

3.1 Installation Procedure

- 1. Upon receipt of the system, carefully check each component against the bill of materials to ensure that everything has been received with the system. If anything is missing or damaged, immediately contact the freight company to file the appropriate claim.
- 2. Remove system from wooden 2 x 4 undercarriage using suitable materials handling equipment.
- 3. Install catcher tank sweeper package as shown in the sweeper layout drawing provided.
- 4. Install the gate valve to the suction port on the catcher tank.
- 5. Install the gate valve to the discharge port on the catcher tank.
- 6. Install hose barbs into the suction and discharge gate valves.
- 7. Close the suction and discharge valves.
- 8. Fill the catcher tank with water.
- 9. Position system next to waterjet machine as discussed with Ebbco Inc. Anchor system to floor as necessary.
- 10. Using the black suction hose and clamps provided in the installation kit, connect the suction barb on the catcher tank to the suction barb on the garnet removal system.
- 11. Using the black discharge hose and clamps provided in the installation kit, connect the discharge barb on the catcher tank to the discharge barb on the garnet removal system.
- 12. Place abrasive bag hopper under purge outlet. Connect decant line to fitting provided on hopper.
- 13. Connect the overflow piping from the 3" port on the abrasive bag hopper to the garnet pump column.
- 14. Have a qualified industrial electrician connect the 3 phase electrical power to the control panel as per electrical drawing. (230vac/3 ph/60Hz)

3.2 Start Up Procedure:

- 1. Check the pump suction basket for debris.
- 2. Open the suction and discharge valves on the catcher tank.
- 3. Ensure that the catcher tank is full of water.
- 4. Check pump for correct rotation (clockwise as viewed from the top of the motor) by bumping the HOA switch, located on the main electrical panel.
- 5. The pump motor on the filtration system has been synchronized at the factory if the pump motor is running in reverse have a qualified electrician swap over one of the in coming line powers at electrical panel.
- 6. Turn the HOA switch to the HAND position.

Warning! If the filtration system dose not prime after 5 seconds, stop the system. Try three more times and if the system still will not prime call the Ebbco service department 1-586-716-5151

7. Check separator inlet and outlet pressure gauges to ensure differential pressure is between 4 and 12 psi.

Section 3: System Installation and Start-Up



Warning If pressure differential is too low or is too high, call the Ebbco service department 1-800-991-4225

Section 4: System Maintenance

4.1 Garnet Removal System Daily Check List

Warning Always disconnect power and relive pressure from the system before performing any maintenance on this filtration system.

Caution Always follow correct lock out procedures when working on this filtration system.

Warning Failure to keep suction above -10 in/hg could result in catastrophic pump failure.

- 1. Make sure suction basket is serviced (empty).
- 2. Open all gate valves.
- 3. Start filtration system.
- 4. Check suction basket pressure gauge. At start up this should read approximately -3 in.hg service basket before the suction vacuum gauge reads -10 in.hg.
- 5. Check inlet and outlet gauges on top of separator. These pressure readings should be approximately 35 psi on the inlet gauge and approximately 26 psi on the outlet gauge. Separator must run between 4 and 12 psid.

Warning This garnet removal separator must run between these pressure differentials. If the system does not maintain the proper differential pressure it will affect the garnet removals performance and can cause premature pump maintenance/failure.

- 6. Service hopper as needed.
- 7. In front of the eductors there will be no garnet accumulation, however there maybe some quite areas in the tank where garnet may collect. The garnet "pile" should not be allowed to exceed 6" in height. Monthly checking of garnet build up on the tank bottom is advised, using a stick tap on the tank bottom in various locations. Any garnet accumulation will show up on the stick and it can be easily removed.

If there are any questions regarding this system please call the Ebbco Service Department at 1-800-991-4225

Section 4: System Maintenance

The system will require the following items to be maintained on a scheduled basis.

Warning Always disconnect power and relive pressure from the system before performing any maintenance on this filtration system.

Caution Always follow correct lock out procedures when working on this filtration system.

4.2 Pump Suction Basket

The vacuum gauge located on the pump suction basket should be monitored every time the system is started and then after every 8 hours of operation to ensure that the suction does not exceed -10 in/hg.

The pump suction basket should be removed and emptied every 8 hours of operation. It is important to check the condition of the gasket on basket's lid, make sure it is free of dirt and is firmly in place before turning the system back on.

Ebbco recommends that a preventive maintenance schedule be implemented for this component.

Note: The vacuum gauge must read -3 in.hg – service basket at -10 in.hg.

4.3 System Pump

The centrifugal pump has been tested and greased at the factory; therefore lubrication is not necessary for a period of approximately six to eight months. Remember that over greasing will cause the bearing to run hot, so grease bearings sparingly when it is necessary. Ebbco recommends the use of sri # 2 chevron ball bearing grease.

Applications were there is a high abrasion the pump may have to be inspected quarterly for wear on impeller and impeller housing.

It is recommended that a routine maintenance schedule be set up and followed for the best service of the pump. A periodic comparison of existing operating conditions and data against data taken when pump was initially started may indicate a problem developing and allow for a planned maintenance check before a breakdown occurs.

4.4 Centrifugal Separator

There is no scheduled maintenance on the separator itself.

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Section 4: System Maintenance

4.5 Work Tank Sweeper Package

To ensure that the garnet removal system works at the designed performance the work tank sweeper package must be visually inspected every 12 months. If the sweeper package is damaged (broken eductor or piping, blocked suction) there will be a noticeable change in system performance. This may manifest itself as a separator inlet pressure drop, a low differential across the separator or a high vacuum gauge reading. If any of these condition occur and are not corrected the system pump and other components will become damaged.



- Once the work tank has drained of water:
- Check for damaged of broken piping and eductors.
- Check for any garnet build up in front of any eductor.
- Check for any material that may be wedged between the eductor nozzle and the horn.

Ebbco Inc can provide an experience service technician to service the tank sweeper package and inspect the complete system. Please call Ebbco for pricing and to schedule a service technician.

4.6 Abrasive bag hopper

The hopper should be visually inspected to be aware of solids level, service when full.

Section 5: Troubleshooting Guide

5.1 System Troubleshooting

Warning Always disconnect power and relive pressure from the system before performing any maintenance on this filtration system.

Caution Always follow correct lock out procedures when working on this filtration system.

1. Pump will not start

a. Check the electrical hookup for proper direction and power requirements.

Warning do not operate the pump without the inner basket inside the strainer

2. No flow/no pressure

- a. Check the electrical hookup for proper direction and power requirements. The pump's motor should run clockwise looking down from the top.
- b. Check fuses in step-down transformer. Replace as necessary.
- c. Check the motor for any foreign objects.

3. Decreasing flow and pressure during operation

a. Check the pump protection strainer for fouling. If plugged, remove the contaminants. Caution: do not operate the pump without the inner basket inside the strainer.

4. Low flow/low pressure (10 psi or less)

- a. Check the rotation of the pump motor. It should be running in the direction noted in 1.a.
- b. Check the pump protection strainer for fouling.

5. No flow/maximum pressure (pegged gauges)

a. Check the separator's purge area for blockage.

6. No transfer of solids/correct separator pressure/correct separator flow

Check for blockage in purge area.

Section 5: Troubleshooting Guide

5.2 System Pump

For troubleshooting pumps, read symptom describing problem, consult keyed causes and correct those that apply. Caution: be sure unit's power is disconnected before attempting any work on pump or motor.

	SYMPTOM	KEY NUMBERS FOR CAUSES
Α	Pump does not deliver liquid	1,2,3,4,6,10,12,14,15,20,21
В	Pump delivers too little flow	2,3,4,5,6,7,10,11,12,13,15,18,20,21,27,28
С	Delivery pressure too low	5,12,13,14,15,18,20,27,28
D	Pump loses prime after starting	2,3,5,6,7,10
Е	Pump needs too much power	13,15,16,17,18,21,22,24,25,27
F	Seal leaks	22,24,29,30
G	Pump vibrates or is noisy	2,3,4,10,19,21,22,23,24,25,26,28,29,30,31,
		32,33,34
н	Motor bearings have short life	22,24,25,26,29,30
I	Pump overheats and/or seizes	1,4,19,20,22,25,26,29,30

	CAUSES		
1	Pump not primed	18	Viscosity of liquid different than design
2	Pump or suction pipe not completely full of liquid	19	Pump operating at very low capacity
3	Suction lift too high	20	Parallel operation of pumps unsuited for such operation
4	Pump cavitating, increase suction pressure	21	Foreign matter in impeller
5	Excessive amount of air/gas in liquid	22	Misalignment of pump or piping
6	Air pockets in suction pipe	23	Foundations not rigid
7	Air leakage in suction pipe	24	Shaft bent
		25	Rotating part rubbing on stationary part
		26	Bearings worn
10	Suction pipe not sufficiently submerged	27	Wear ring worn
11	Impeller, suction or trap partially or completely plugged	28	Impeller damaged
12	Speed too low	29	Shaft running off center due to worn bearings or misalignment
13	Voltage wrong or too low	30	Impeller out of balance resulting in vibration
14	Wrong direction of rotation	31	Excessive grease in bearing causing high bearing temperature
15	System head too high for pump design	32	Lack of lubrication
16	System head too low for system design	33	Dirt in bearings
17	Specific gravity of liquid different than design	34	Rust in bearings due to water getting into motor

Section 6: Parts List

REC. ON SITE	QTY REQ.	DELIVERY TIME	COMPONENT DESCRIPTION	LOCATION OF PART ON SYSTEM	PART NUMBER
N/A	1	2-4 weeks	Centrifugal separator	On separator support frame.	SDS-0250-B
N/A	1	2-4 weeks	Complete pump	On pump base.	PCL2x3-10-B-CC+6
1	1	2-4 weeks	Pump impeller	Inside pump impeller housing.	PCL2x3-10-B-CC+6- IMP.10"
1	1	Stock 2-5 days	Pump case gaskets	Inside pump impeller housing.	61115
1	1	Stock 2-5 days	Pump strainer basket's internal basket	Inside pump suction strainer.	PKG-98-IB-SS
1	1	Stock 2-5 days	Pump strainer basket's lid gasket	On suction basket lid.	U9-46
2	2	Stock 2-5 days	0-60 psi liquid filled pressure gauge	Separator inlet/outlet.	GRS-60-GA
1	1	Stock 2-5 days	Vacuum gauge -30 in/mg 0PSI	On side of pump suction strainer basket.	GRS-V-GA
N/A	1	Stock 2-5 days	Abrasive bag hopper bag	In abrasive bag hopper.	GRS-ABH-B
12	12	Stock 2-5 days	3/8" poly eductor	End of clean discharge in system tank.	0MP

Section 7: General Policy & Limited Warranty

It is Ebbco's policy to ship and charge for replacement parts upon notification of a problem. Warranty will be determined upon inspection of said part after it is returned to Ebbco, freight pre-paid. A returned goods claim form will be sent with replacement part and must be returned with defective part. Ebbco Inc. shall not be liable for incidental and consequential losses and damages under this expressed warranty, any applicable implied warranty, or claims for negligence.

All products manufactured and marketed by Ebbco are warranted to be free of defects in materials and workmanship for a period up to one year for date of delivery or 2080 hours of operation, whichever comes first.

Equipment such as pumps, pump bodies, separators, etc. will carry one-year manufacturer warranty. Pump seals: Ninety day limited warranty.

This limited warranty does not cover any products, damages or injuries resulting from misuse, neglect, normal expected wear, chemical-caused corrosion, improper installation or operation contrary to Ebbco's recommendations. Nor does it cover equipment which has been modified, tampered with or altered without authorization.

No other extended liabilities are stated or implied and this warranty in no way covers incidental or consequential damages, injuries or cost resulting from any such defected product.

Product Profile

HEAVY DUTY SUCTION STRAINER BASKET

MODEL # PKG98 & PKG51

PRODUCT FEATURES

THE HEAVY DUTY SUCTION STRAINER BASKET IS USED AS THE FRONT LINE PUMP PROTECTION. EBBCO INC SUCTION STRAINER BASKET HAS A RUGGED ONE PIECE CAST IRON BODY WITH A CAST IRON LID. BASKET MATERIAL AS STANDARD ON THE PKG-51 IS ABS AND STAINLESS STEEL GR303 ON THE PKG-98. A STAINLESS STEEL BASKET IS PROVIDED AS AN OPTION FOR THE PKG-51.

ALL LID GASKET MATERIAL IS BUNA-NITRILE AS STANDARD WITH EPDM AND VITON AS OPTIONS.

- RUGGED CAST IRON HOUSING.
- PKG-98 STAINLESS STEEL PERFORATED BASKET.
- PKG-51 ABS INTERNAL PERFORATED BASKET. OPTIONAL STAINLESS STEEL.
- BUNA-NITRILE LID GASKET.



MODEL PKG98







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Specifications

HEAVY DUTY SUCTION STRAINER BASKET

MODEL # PKG98 & PKG51

RECOMMENDED	PKG-51 GPM	PKG-98 150 GPM
MAX FLOW RATE MAX TEMP	180°F	300 GPM 180°F
OUTLET MATERIALS OF	SQ. FLANGE	SQ. FLANGE
CONSTRUCTION		
LID O-RING BASKET	CAST IRON CAST IRON BUNA-N ABS (OR SS)	CAST IRON CAST IRON BUNA-N SS

MODEL #PKG-98



SPARE PARTS

O-RING	U9-46	U9-171
FLANGE	C20-19	C20-19
GASKET		
LOCK HANDLE	C154-18D	C154-18D
LID	C3-30	C3-105
ABS BASKET	C108-11P	N/A
SS BASKET	C108-11SS	16401-0030



3.5" 🕇

MODEL #PKG-51





MAINTENANCE • INSTALLATION • OPERATION

7550 SERIES 52 HEAVY DUTY, 53 HEAVY DUTY AND 54 HEAVY DUTY POWER FRAMES

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WARRANTY

Gusher Pumps, Inc. will replace or repair, within one year of shipment from our plant, any pump in our judgement that has failed due to defects in materials or workmanship, provided the pump has been properly installed and maintained and has not been subject to abuse. These pumps must return to Gusher Pumps, Inc. with complete history of service for inspection and warranty consideration. Gusher Pumps, Inc. does not accept the responsibility for transportation to and from our plant. Furthermore, we do not assume any responsibility for consequential damage or loss of production.

RECEIVING AND INSPECTION

The utmost care has been taken at the factory to assure proper coupling alignment and impeller adjustment. However, due to circumstances beyond our control, YOU MUST inspect the pump upon receipt and follow the installation instructions completely before start-up.

RECEIVING:

- 1. Rotate shaft by hand. If it does not rotate freely:
 - a. Check impeller adjustment.
 - b. Check for bent coupling guard.
 - c. Check slinger (#8).
 - d. Check for bent shaft (#1).
- Check for cracked or damaged parts. If upon receipt, you find the pump damaged, file a claim with the delivering carrier.

- If drive motor has been supplied, check the R.P.M. and horsepower to be sure it is correct as ordered.
- Check the pump name tag to be sure we have shipped correctly as ordered:
 - a. Model Number
 - b. Head in feet (Ft. Hd.)
 - c. Gallons per minute (G.P.M.)
 - d. Construction:
 - 1. All iron.
 - 2. All iron with stainless steel shaft and impeller.
 - 3. All stainless steel.
- If there is anything that appears to be incorrect, call the factory immediately.

INSTALLATION

After careful preliminary inspection, you may proceed with the installation of the pump into your system.

- 1. Lower the pump into system.
- Make sure mounting plate (#37) is setting firmly on the support channels. (It may be necessary to use metal shims to level plate.)
- Secure mounting plate (#37) by using hold-down screws in all four corners. Again, care must be taken to make sure plate is firm and level. DO NOT force bowed plate level. Use metal shims if necessary.
- 4. Making pipe connections:
 - Extreme care must be taken to support piping without causing any strain on the pump.
 - Install pipe hanger on the discharge pipe so all piping weight is supported by the hanger and not be the pump or the casing.
 - Bolt holes must line-up without prying to insert bolts.
 - d. When tightening flange bolts, pipe flanges must not be forced together.
 - e. Check valve should be placed in discharge line between gate valve and pump discharge pipe to prevent liquid from running back through the pump and causing reverse rotation. This is extremely important in applications with intermittent duty where the pump may be rotating backwards when service is resumed. This will cause damage to the pump and the drive motor.
 - Pressure gauge should be located at the pump discharge, as all performance data is taken at pump discharge.
 - g. If intake piping is used to pump the tank down, It must also be supported independently of the pump.
- Remove coupling guard and rotate coupling by hand. Pump should rotate freely at this point. If it does not, check for:
 - Piping strain: without exception, piping must not rest on pump in any manner. (SEE ITEM #4 of the INSTALLATION SECTION.)
 - b. Impeller adjustment:
 - Disconnect coupling (#32) and remove sleeve (#32a).
 - 2. Loosen three locking screws (#57).
 - Loosen three adjusting screws (#55).
 - Lightly tap shaft (#1) until impeller (#12) bottoms on the intake flange (#13).



- Tighten three adjusting screws by hand until they touch ball bearing housing (#5).
- Tighten three adjusting screws 1/4 turn (approximately .016*) by alternating from one screw to the next, until all three screws have been turned 1/4 turn.
- Tighten locking screws (#57) and jamb nuts (#56).
- Rotate coupling by hand to be sure impeller (#12) does not rub intake flange (#13). If impeller does rub, repeat steps #1 through #7.
- 9. Connect Coupling.
- c. Slinger adjustment: The slinger (#8) is set at the factory and normally causes no problems, but should be checked when unit is inspected upon arrival at your plant site and before unit is lowered into position in your system.
- d. Coupling alignment SEE ITEM #6 below:
- Coupling alignment: MUST BE CHECKED before and after system start-up.
 - a. Check parallel alignment by placing a straightedge across the two coupling flanges and measuring the maximum offset at various points around the periphery of the coupling. If the maximum offset exceeds .010", realign the coupling.



b. Check angular alignment with a micrometer or caliper. Measure from the outside of the one flange to the outside of the other at intervals around the periphery of the coupling. Determine the maximum and minimum dimensions. DO NOT rotate. The difference between the maximum and the minimum must not exceed .010". If a correction is necessary, be sure to recheck the parallel alignment.



CHM STYLE ONLY (chair mounted style)

- c. If coupling alignment is out, adjustment can be made by the following steps.
 - 1. LATERAL PARALLEL MISALIGNMENT is adjusted by loosening the four motor retaining bolts (#49) after which you loosen the lateral adjusting screws (#58) on the side of the motor that has to be shifted and tighten the remaining lateral adjustment screws until lateral parallel alignment is achieved. (SEE FIG #3) If misalignment is our more than .020" SEE #5.



- 2. HORIZONTAL PARALLEL MISALIGNMENT is adjusted by loosening the four motor retaining bolts (#49) after which you add or subtract shims from between motor base and motor support pads (#50). (SEE FIG #2) If more .1875 of an inch total shims are required or alignment cannot be achieved without any shims, SEE #5. Tighten all screws before operating pump.
- 3. LATERAL ANGULAR MISALIGNMENT is adjusted by loosening the four motor retaining bolts (#49) after which you loosen the angular alignment screws (#59) on the side of motor that has to be lowered and tighten the angular alignment screws on side of motor that has to be raised, until angular alignment is achieved. (SEE FIG #3) Tighten all screws before operating.
- 4. HORIZONTAL ANGULAR MISALIGNMENT is adjusted by loosening the four motor retaining bolts (#49) after which you add or subtract shims from between motor base and motor support pads (#50). (SEE FIG #2) Tighten all screws before operating pump.
- 5. If lateral alignment and horizontal parallel alignment cannot be achieved with the above steps use the following operation. Loosen nuts or screws that hold bearing housing to mounting plate. Tap ball bearing housing (#5) with lead hammer to move coupling into alignment. If unable to align coupling by tapping the ball bearing housing then insert a prybar between the ball bearing housing and the burned out hole in the mounting plate (#37) and shift coupling into alignment by prying housing from one position to another as required. Tighten all screws before operating pump.

NOTES:

1. DO NOT LOOSEN THE FOUR MOTOR SCREWS TO MUCH, AS THIS WILL CAUSE DIFFICULTY WHEN TRYING TO ALIGN COU-PLING. Motor screws must be snug so a slight force must be applied to move motor.



LATERAL PARALLEL MISALIGNMENT LATERAL ANGULAR MISALIGNMENT FIG. #3

- 2. If an adjustment in either parallel or angular alignment is required, you must check both after adjustment is made.
- 3. Coupling alignment must be checked after system has been operating for 300 hours. Then as a preventative maintenance procedure, it should be checked every 1200 hours of normal operation. More sever duty operation requires more frequent attention.
- Make electrical connection to conform with state and local codes. (It is advised to use approximately 4' length of flexible conduit to facilitate removal of chair, if repair is required.)

Upon initial start-up, pumps may seem to run tight and hot. This is caused by breaking-in of oil seals and ball bearings. Pump will operate normally after approximately 150 hours of service. Ball bearings should not run over 225° F. When checking temperature use a pyrometer.

MAINTENANCE

 Lubrication – all pumps are lubricated at the factory and should not require additional lubrication for approximately 1200 hours of run at 1750 R.P.M. OR 600 hours if run at 3450 R.P.M. A well planned maintenance schedule can only be devised after careful observation of the pump for the first six months of operation and the lubrication that has been required. Each pump installation is unique and requires a different lubrication schedule compatible with that specific operation. Use Chevron SRI #2 ball bearing grease. DO NOT OVER GREASE as it will cause ball bearings to run hot.

To lubricate:

- a. Remove pipe plug from back of ball bearing housing (#5).
- b. Fill with grease until fresh grease flows from opening.
- c. If automatic lubrication system is being used, reliefs must be placed in the tapped hole (1/8" N.P.T.).
- 2. Coupling alignment: This must be checked before and after system start-up; after 300 hours of operation; and again after 1200 hours of operation. Follow procedure given in ITEM #6 of the INSTALLATION SECTION of this manual. Again, we recommend strongly that a routine preventative maintenance schedule be devised and followed to achieve optimum life and performance from the pump.

DISASSEMBLY

A. CHAIR AND DRIVE MOTOR

- 1. Disconnect electrical leads. During installation it was advised to allow sufficient flexible conduit (approximately 4 feet) to allow removal without disconnection of electrical leads.
- Remove coupling guard.
- 3. Disconnect coupling (#32).
- 4. Remove four motor retaining bolts (#49). Motor can now be removed from chair.
- 5. Break welds loose that hold discharge pipe cover plate to mounting plate (#37).
- Remove bolts & nuts that hold discharge pipe to impeller housing (#11).

7. Remove discharge pipe.

- 52VHD Power Frame
 - a. Remove bolts, nuts & washer that hold chair (#34) to stem (#7).
 - b. Remove chair (#34) from pump.

53VHD & 54VHD Power Frames

- Remove intake flange (#13).
- NOT APPLICABLE ON ALL MODELS.
- b. Remove impeller housing (#11).
- c. Remove impeller retaining nut (#40).
- Remove impeller retaining washer (#18). NOT APPLICABLE ON ALL MODELS.
- Remove impeller (#12).
- f. Remove impeller drive key (#19) and tape it to the hub of the impeller so it will not get lost.
- g. Loosen set screws in slinger (#8).
- h. Remove stem plate (#41).
- NOT APPLICABLE ON ALL MODELS. i. Remove stem (#7).
- j. Remove power frame assembly from chair (#34).

- B. BARREL AND DRIVE MOTOR
 - 1. Disconnect electrical leads. During installation it is advisable to allow sufficient flexible conduit (approximately 4 feet) to allow removal without disconnection of the electrical leads.
 - 2. Remove coupling guard.
 - 3. Disconnect coupling (#32).
 - 4. Remove bolts that hold barrel (#36) to bearing housing (#5).
 - 5. Remove barrel (#36) & motor from power frame.
- C. PUMP DISASSEMBLY

Read thoroughly before disassembly.

- 1. 52VHD barrel mount or chair mount.
 - a. Follow steps in section A or B
 - b. Remove bolts nuts and washers that hold discharge pipe to the impeller housing (#11). Remove bolts, nuts and washers that hold mounting plate (#37) to stem (#7). Remove mounting plate (#37). (Barrel mount only.)
 - c. Remove intake flange (#13) NOT APPLICABLE ON ALL MODELS.
 - d. Remove impeller housing (#11).
 - e. Remove impeller retaining screw (#16).
 - Remove impeller retaining washer (#18).
 - g. Remove impeller (#12).
 - h. Remove impeller drive key (#19). Tape it to the hub of the impeller so it will not get lost.
 - i. Loosen set screw in slinger (#8).
 - Remove stem plate (#41). 1. NOT APPLICABLE ON ALL MODELS.
 - k. Remove stem (#7).
 - Remove ball bearing retainer (#2).
 - m. Slide shaft (#1), telescoping ball bearing housing (#5a), ball bearing (#6), grease and radial bearing retainer (#61) and radial bearing (#4) out of bearing housing (#5) as one unit.
 - n. Remove ball bearing lock nut (#3) from shaft (#1).
 - o. Remove ball bearing (#6) from shaft (#1).
 - p. Remove telescoping ball bearing housing (#5a) from shaft (#1).
 - g. Remove oil seal (#21) from telescoping ball bearing housing (#5a).
 - Remove grease and radial ball bearing retainer (#61) and radial ball bearing (#4) together from shaft (#1).
 - s. Remove oil seal (#22) from ball bearing housing (#5).
 - Remove throttle bushing retainer (#9). t. . NOT APPLICABLE ON ALL MODELS.
 - u. Remove throttle bushing (#10).

- 2. 53VHD & 54VHD chair mount.
 - a. Follow steps in section A.
 - b. Remove 3 bolts (#57). SEE FIG #1.
 - c. Slide shaft (#1), ball bearing retainer (#2), thrust ball bearing (#6) and radial ball bearing (#4) out of ball bearing housing (#5) as one unit.
 - d. Remove ball bearing retainer (#2).
 - Slide telescoping ball bearing housing (#5a) down off of the thrust bearing (#6).
 - Remove ball bearing housing (#3) from shaft (#1).
 - g. Remove thrust ball bearing (#6) from shaft (#1).
 - h. Slide telescoping ball bearing housing (#5a) off shaft (#1).
 - Remove bearing and grease retainer (#61) and radial ball bearing (#4) from shaft (#1). Remove both at the same time so as not to damage retainer.
 - Remove oil seal (#21) from telescoping ball bearing housing (#5a).
 - k. Remove oil seal (#22) from ball bearing housing (#5).
 - Remove throttle bushing retainer (#9). NOT APPLICABLE ON ALL MODELS.
 - m. Remove throttle bushing (#10).
- 3. 53VHD & 54VHD barrel mount
 - a. Follow steps in section B.
 - Break welds loose that hold discharge pipe cover plate to mounting plate (#37).
 - c. Remove bolts and nuts that hold discharge pipe to impeller housing (#11).
 - d. Remove discharge pipe.
 - Remove intake flange (#13).
 NOT APPLICABLE ON ALL MODELS.
 - Remove impeller housing (#11).
 - g. Remove impeller retaining nut (#40).
 - Remove impeller retaining washer (#18). NOT APPLICABLE ON ALL MODELS.
 - Remove impeller (#12).
 - Remove impeller drive key (#19) and tape it to the hub of the impeller so it will not get lost.
 - k. Loosen set screws in slinger (#8).
 - Remove stem plate (#41). NOT APPLICABLE ON ALL MODELS.
 - m. Remove stem (#7)
 - n. Remove power frame from mounting plate (#37)
 - Remove 3 bolts (#57). SEE FIG #1.
 - p. Slide shaft (#1), ball bearing retainer (#2), thrust ball bearing (#6) and radial ball bearing (#4) out of ball bearing housing (#5) as one unit.

- q. Remove ball bearing retainer (#2).
- r. Slide telescoping ball bearing housing (#5a) down off of the thrust bearing (#6).
- Remove ball bearing lock nut (#3) from shaft (#1).
- Remove thrust ball bearing (#6) from shaft (#1).
- Slide telescoping ball bearing housing (#5a) off shaft (#1).
- Remove bearing and grease retainer (#61) and radial ball bearing (#4) from shaft (#1). Remove both at the same time so as not to damage retainer.
- w. Remove oil seal (#21) from telescoping ball bearing housing (#5a).
- Remove oil seal (#22) from ball bearing housing (#5).
- y. Remove throttle bushing retainer (#9). NOT APPLICABLE ON ALL MODELS.
- Remove throttle bushing (#10).

TO REASSEMBLE PUMP REVERSE THE PRO-CEDURE USED WHILE MAKING SURE OF THE FOLLOWING.

- For bearing installation see page 7.
- Check grease seals (#21) and (#22) for wear. Replace if worn.
- Install retainer (#61) and telescoping ball bearing housing (#5a) on shaft (#1). Before putting bearing (#6) on shaft (#1).
- Install slinger (#8) on shaft (#1) while connecting stem (#7) to bearing housing (#5).
- Check throttle bushing for wear. Replace if worn. There are two different versions of throttle bushings. One is a TEFLON TYPE that has a retainer. The other is a CARBON TYPE that is pressed in place.
- Clearance between impeller and housing or intake flange should not exceed .015". To adjust clearance see INSTALLATION on page 3, section 5b (for SE models only).

CERTAIN MODELS HAVE AN ENCLOSED IM-PELLER. THESE MODELS ARE SUPPLIED WITH A CARBON WEAR RING (#27) THAT IS PRESS FITTED INTO THE INTAKE FLANGE (#13). UPON DISAS-SEMBLY CHECK THE WEAR RING FOR WEAR. RE-PLACE IF WORN.

BEARING INSTALLATION

Begin by cleaning your work area thoroughly, contaminants can cause bearing failures as fast as any other reason.

When a bearing is installed, the mounting force should be applied against the ring, and only the ring, which is being press-fitted. A bearing should never be forced onto a shaft by pressure or hammer blows applied to the other ring, nor should the bearing be press-fitted into housing by force allied to the inner ring.

Using an arbor press, the bearing may be laid on a face block which contacts only the bearing inner ring and which has a hole diameter greater than the bearing bore, as shown in FIG. 10. The shaft is pressed through the bearing until it is seated firmly against the shaft shoulder.

If the shaft is not too long, it can be supported beneath the table of the arbor press and the bearing pressed onto it by ram pressure against a piece of soft metal tubing, as shown in FIG. 11. The tubing must be clean, inside and out, and the diameter of the tubing should be slightly greater than the bearing bore. The end of the tubing should be square (with corners chamfered to avoid flaking) and should contact only the bearing inner ring. The shaft must be held in line with the ram of the arbor press to avoid cocking the bearing on the shaft seat.

When an arbor press is not available, the bearing can be driven onto the shaft seat by light hammer blows against the end of the soft metal tubing. These blows should be made alternately against opposite sides of the tubing face, and great care must be taken to avoid cocking the bearing as it is driven onto the shaft seat.

When a ball bearing is installed into the housing it is normally a slip fit, however if force is necessary to install bearing the force should be exerted on the outer ring of the bearing as shown in FIG. 12. Again the force must be applied evenly so as not to cock the bearing in the bore.



TROUBLE SHOOTING

NO WATER DELIVERED.

(1) Pump not primed.

- + (2) Speed to low.
 - (3) Discharge head too high.
 - (4) Suction line or suction strainer is clogged.
 - (5) Impeller completely clogged.
 - (6) Wrong direction of rotation.
 - (7) Too much clearance between impeller and intake flange.

NOT ENOUGH WATER DELIVERED.

- Air leaks in suction or stuffing boxes.
- + (2) Speed too low.
 - (3) Discharge head higher than anticipated.
 - (4) Too much clearance between impeller and intake flange.
 - (5) Impeller partially clogged.
 - (6) Not enough suction head for hot water.
 - (7) Mechanical defects:
 - Wear ring is worn.
 - Impeller damaged.
 - (8) Impeller diameter too small.
 - (9) Foot valve too small.
- (10) Foot valve or suction opening not submerged deep enough.

NOT ENOUGH PRESSURE.

- + (1) Speed too low.
 - (2) Air in water.
 - (3) Mechanical defects: Wear ring is worn.
 - Impeller damaged.
 - (4) Impeller diameter too small.

VIBRATION.

- (1) Bent shaft.
- (2) Pipe strain.
- (3) Impeller clogged.
- (4) Coupling alignment off.

PUMP WORKS FOR A WHILE AND THEN LOSES SUCTION.

- (1) Leaky suction line.
- (2) Water seal plugged.
- (3) Impeller clogged.
- (4) Air or gasses in liquid.

PUMP TAKES TOO MUCH POWER.

- + (1) Speed too high.
 - (2) Head lower than rating, pumps too much water.
 - (3) Specific gravity or viscosity too high.
 - (4) Mechanical defects: Shaft bent. Power frame in bind.
 - Wear ring is worn.
 - (5) Impeller diameter too large.
 - (6) Pump delivering too many gallons.

+ When directly connected to electric motors, check for full voltage across all electrical leads.



9

53HD & 54HD POWER FRAME

n



10

Madel	#11 Impeller Housing	#12 Impeller	#13 Intake Flange	#27 Wear Ring	#38 Impeller Hsg. Gasket	#39 Stem Pit. Gasket	841 Stem Plate
1.25X1.5-7	27037	25015	33015	-	61013	61149	21037H
1.5X2-7	27039	25016	33016		61013	61149	21037H
ZX2.5-7	27041	25017	33017	1.14	61013	61149	21037H
2.5)(3-7	27043	25018	33018	-	61013	61149	21037H
3X4-7	27013	25013	33013	-	61013	-	-
4X5-7	27047	25020	33020	-	61013	61149	21037H
CL-3X4-8	27108A	25108	-	-	61108	-	21108H-4
1.25X1.5-9	27038	25011	33011	-	61011	61011	21038H
506-9	27049	25022	33022	-	61011	61011	21038H
1.5X2-10	27040	25009	33009		61007	61007	21040H
CL-1.5X3-10	27111A	25111	-	-	61115	-	21111H
2X2.5-10	27042	25010	33010	-	61007	61007	21040H
2.503-10	27044	25007	33001	-	61007	61007	21040H
3X4-10	27046	25006	33000	-	61007	61007	21040H
CL-4X6-10	27115A	25115	-		61115	-	21220H
506-10	27053	25023	33023	65012	61007	61007	21040H
40(5-11	27048	25008	33008	-	61008	61008	21048H
6008-11	27300-1	25027	-	-	61006		21048H-1
CL-1.5X3-13	27116A	25416	-	-	61116	-	21173H
30(4-13	27051-1	25019	33019	65019	61012	61012	21051H
CL-3X4-13	2711BA	25118	-	-	61116	-	21140H
4X5-13	27052-1	25021	33021	65019	61012	61012	21051H
CL-4X5-13	27119A	25119	-	-	61116	-	21170H
5X6-13	27154	25012	33012	65012	61012	51012	21051H
CL-6XB-13	27120A	25120	-	-	61116	-	-
606-14	27024	25024	-	-	61024	-	-
CL-6x8-15	27122A	25122	-	-	61122	+	-
CL-5X6-16	27141A	25141	-	65141	61141	-	

Part #	Description	52VHD Power Frame	S3VHD Power Frame	S3VHD Power Frame 6X5-14E	54VHD Power Frame
1	Shaft	7600HD	100025	100034	100035
2	Ball Brg. Retainer	14003	14083	14083	14082
3	Lock Nut	68100	68100-1	68100-1	68100-2
4	Radial Ball Brg.	41211	41316	41316	41319
5	Ball Brg. Housing	51079	51080	51060	51081
54	Telescoping Ball Brg. Housing	51019	51063	51083	51082
6	Trust Ball Brg.	41308-DR	41312-DR	41312-DR	41314-DR
8	Silnger	58002	58055	58065	58054
9	Bushing Retainer	71003	71003-1	71024	71091
10	Throttle Bushing (Teflon)	62001	62001-7	62024	62054
10	Throttle Bushing (Carbon)	62001-C	62025		62054-C
14	Slinger		58053	58053	58071L
16	Impeller Retaining Screw	68015	-	-	
18	Impeller Retaining Washer	68004	-	-	68024-3
19	Impeller Drive Key	71099	71099-1	71099-1	71099-1
21	Oil Seal	83000	83010	83010	83012
22	Oil Seal	83006	83011	83011	83013
40	Impeller Retaining Nut		71213	71213	71213
61	Grease & Radial Brg. Retainer	14079	14080	14080	14081

Model	#7 Stem						
	52VHD	53VHD	54VHD				
1.25X1.5-7	17005	17171	-				
1.5X2-7	17005	17171	+				
202.5-7	17005	17171	-				
2.5X3-7	17005	17171	~				
3X4-7	17005	17171	-				
4X5-7	17005	17171	-				
CL-3X4-8	17005	17171	-				
1.25X1.5-9	17005	17171	-				
5X6-9	17005	17171	-				
1.5X2-10	17005	17171	-				
CL-1.5X3-10	17005	17171					
202.5-10	17005	17171	-				
2.5X3-10	17005	17171	-				
3064-10	17005	17171	-				
CL-406-10	17005	17171	-				
5X6-10	17005	17171	· +				
4X5-11	17005	17171	-				
6X8-11	17005	17171	-				
CL-1.5-3-13	17005	17171	-				
3X4-13	17005	17171	-				
CL-3X4-13	17005	17171	-				
4X5-13	17005	17171	-				
CL-406-13	17005	17171	-				
5X8-13	17005	17171	-				
CL-608-13	-	17209	17210				
6008-14	-	17170	17173				
CL-6068-15	-	17265	17261				
CL-5X5-16		17143	17268				

Frequently Used Formulas & Equivalents

HEAD & PRESSURE FORMULA	$\begin{tabular}{lllllllllllllllllllllllllllllllllll$
Head in feet = $\frac{(\text{Head in psi}) \times 2.31}{(\text{Sp. Gr.})}$	$ \begin{array}{l} h_{a} = \mbox{the absolute pressure in feet of liquid on the surface of the supply liquid.} \\ h_{v} = \mbox{the vapor pressure of the liquid being pumped expressed in feet of head.} \\ h_{s} = \mbox{the height in feet of the supply liquid surface with respect to the pump inlet.} \\ h_{f} = \mbox{suction line friction losses expressed in feet of head.} \end{array} $
Head in psi = $\frac{(\text{Head in ft}) \times (\text{Sp. Gr.})}{2.31}$	These calculations yield the available net positive suction head for a given system. This must be compared to the required net positive suction head NPSH _R calculated by the manufacturer. NPSH _A must exceed NPSH _R .
PRESSUF	RE EQUIVALENT TABLE

Convert to Convert tom	to inf	b/tr	Atmos- pheres	kg/cm ⁴	kgim/	in. willior (SEF)*	R. wztor (68F)#	in. mercury (32F)	mercury (32F)	Bars	Mega- Pascals (MPa) 4
bint bint kmosphyres ugint ² n, water ⁴ n, metcury nm metcury Bass MPa	1 0.0009444 14.696 14.2223 0.021422 0.039092 0.432781 0.491154 0.491154 0.491154 0.491154 14.5038 14.5038	144 1 2116.22 2048.155 0.204768 5.1972 62.3205 70.7242 2.78450 2098.55 20985.5	0.088046 0.090473 1 0.96784 0.090968 0.002454 0.022454 0.022454 0.023421 0.003421 0.003423 0.003423 0.003423 0.00582 9.9692	0.070007 0.000488 1.0332 1 0.0001 0.00253 0.00453 0.00453 0.001566 1.01972	703.070 4.88241 10322.27 10000. 1, 25.375 304.275 345.316 13.56569 76197.2 101972.0	27.7278 0.1825 407.484 294.58 0.00644 1, 12, 13,6185 0.50016 402.156 4021.56	2,3106 0,01605 33,8670 32,8650 0,002287 0,08333 1, 1,1349 0,044690 30,5130 30,5130	2.03602 0.014139 29.921 28.959 0.032896 0.073430 0.88115 1. 0.039837 29.5300 295.300	51.7150 0.35813 760 735.558 0.073558 1.8651 22.3613 25.4005 1. 750.062 750.62	0.06695 0.000479 1.01325 0.96067 0.000098 0.029830 0.029830 0.033854 0.031333 1. 10.0	0.006895 0.0000479 0.101325 0.090067 0.000298 0.0029839 0.0029839 0.0029839 0.0029839 0.0029839 0.0029839 0.0029839 0.0029839 0.0029839 0.0029839 0.0029839 0.0001333 0.10

*Water at 66F (20 C) + mercury at 32F (0 C) Courtesy of Crane Co. Technical Paper 410.

	F	LOW EQUI	VALENTS			
Convert to tram	U.S. gaV min.	imp. galv min.	U.S. million gal/day	Cu. ft. per. sec. (secft.)	Cu. meters per. hour	Liters per. sec.
U.S. gal/min	1. 1.201 894.4 448.83 16852 264.2 4.403 15.85 0.2642	0.8327 1. 578.25 373.7 13200 220 3.67 13.20 0.220	0.00144 0.00173 1. 0.646 22.83 0.3804 0.00634 0.0228 0.000380	0.00223 0.002676 1.547 1. 35.35 0.5886 0.00982 0.0353 0.000589	0.2271 0.2727 157.7 0.060 3600 560.0 1 3.60 0.060	0.0631 0.0758 43.8 28.32 1000 16.667 0.2778 1 0.0167

Convert		Volume and weight equivalents—any liquid							r at 60% (15.6%)
Convert. from	U.S. gallons	Imperial gallons	Cubic inches	Cubic feet	Liters	Gubic maters	Pounds	U.S. tons	Kilo- grams
U.S. gallons Imperial gallons Cubic inches Cubic teet Liters Cubic meters Pounds' U.S. tons"	1. 1.20094 0.004329 7.48052 0.2542 264.2 0.1199 239.87 0.2644	0.8327 1. 0.003605 6.229 0.2200 220.0 0.09987 198.7 0.2202	231. 277.39 1. 1728 61.024 61.024 27.71 55409 61.08	0.13368 0.16054 0.0005787 1. 0.035315 35.315 0.016033 32.066 0.03534	3.7854 4.546 0.016387 29.317 1. 1000. .4539 907.9 1.000	0.0037854 0.004546 0.00016387 0.02832 0.001 1. .000454 0.908 .001	8.338 10.0134 0.036095 62.3714 2.2029 2202.65 1. 2000 2.205	0.00417 0.005 55409 0.03119 0.0011 1.10133 0.0005 1. 0.0011	3.782 4.542 0.016372 28.291 0.1000 1000.0 0.45359 907.2 1

VACUUM PRESSURE EQUIVALENTS

1 atmosphere = 29.92 in Hg = 760mm Hg = 14.7 psi

- 1 mm Hg = 1 Torr = (3.937 x 10⁻⁹) in Hg = 1000µHg = 1.333 millibars
- 1 bar = 103 millibars = 104 microbars = 750.06 mm Hg
- 1 microbar = 0.75 micron
- 1 inch Hg = 2.54 x 101 mm Hg

x in. Hg vacuum = (29.92 - x) in Hg absolute y mm Hg vacuum = (760 - y) mm Hg absolute z PSIG = (z + 14.7) PSIA W PSIA = (w - 14.7) PSIG

CHART II

VISCOUS LIQUIDS VISCOSITY MEASURES A LIQUID'S RESISTANCE TO FLOW

			VISCOSITY C	ONVERSION	TABLE		
SAYBOLT UNIVERSAL SSU	STOKES	CENTI	POISES*	CENTI* POISES	ENGLER	REDWOOD NO. 1 SECONDS	TYPICAL LIQUIDS AT 70° F
31	.010	1.00	.008	.8	54	29	WATER
35	.025	2.56	.020	2.05	59	32.1	KEROSENE
50	.074	7,40	.059	5.92	80	44.3	NO. 2 FUEL OIL
80	.157	15.7	.126	12.6	125	69.2	NO. 4 FUEL OIL
100	_202	20.2	.162	16.2	150	85.6	TRANSFORMER OIL
200	.432	43.2	.346	34.6	295	170	HYDRAULIC OIL
300	.654	65.4	.522	52.2	470	254	SAE 10W OIL
500	1.10	110	.88	88.0	760	423	SAE 10 OIL
1,000	2.16	220	1.73	173	1,500	896	SAE 20 OIL
2,000	4.40	440	3.52	352	3,000	1,690	SAE 30 OIL
5,000	10.8	1,080	8.80	880	7,500	4,230	SAE 50 OIL
10,000	21.6	2,160	17.0	1,760	15,000	8,460	SAE 60-70 OIL
50,000	108	10,800	88	8,800	75,000	43,660	MOLASSES B
100,000	216	21,600	173	17,300	150,000	88,160	MOLASSES C

*Poises and centipoises are given for oil of .8 spec. Gravity, Relationship: centistokes X specific gravity = centipoises.

PUMPING VISCOUS LIQUIDS WITH CENTRIFUGAL PUMPS

VISCOSITY SSU	30	100	250	500	750	1000	1500	2000
Flow Reduction GPM %	-	3	8	14	19	23	30	40
Head Reduction Feet %		2	5	11	14	18	23	30
Horsepower Increase %	-	10	20	30	50	65	85	100

CONVERSION CHART

BARS		х	14.5		LBS / SQ. INCH
CELSIUS		-	.556 X	(0F -	- 32)
CUBIC METRE F	PER HOUR	x	4.403	-	GALLONS-U.S. PER MINUTE
FAHRENHEIT		-	(1.8 x °c)	+	32
FEET		х	.3048	-	METERS
FEET OF WATER	1	x	.4335	=	LBS / SQ. INCH
GALLONS-IMP	ERIAL	x	1.20095	-	GALLONS-U.S.
GALLONS-U.S.		×	.83267	-	GALLONS-IMPERIAL
GALLONS-U.S.		x	3.785	-	LITRES
GALLONS-U.S.	PER MINUTE	x	.2271	-	CUBIC METRE PER HOUR
HORSE POWER		×	.746	-	KILOWATT
INCHES		x	25.4	-	MILLIMETRES
KILOWATT		x	1.34048	-	HORSE POWER
LITRES		×	.2642	-	GALLONS-U.S.
METRES		х	3.281	-	FEET
MILLIMETRES		х	.03937	-	INCHES
POUNDS / SQ. II	NCH	х	2.307	-	FEET OF WATER
POUNDS / SQ. II	NCH	x	.0689	-	BARS





ENGINEERING DATA

CAPACITY AND HEAD IN FEET... Gallons per minute (G.P.M.) and Foot heads in the performance charts in this catalog were compiled from actual tests. The Maximum G.P.M. shown is the pump capacity at rated horsepower. The maximum Head in Feet is at full rated speed (60 cycle current). For Maximum G.P.M. all piping should be straight, short and large as possible. Heads and G.P.M. are based on tests with specific gravity of 1 and a temperature of 70°F.

HOW TO FIGURE HEAD ...

- 1. Determine static lift (height liquid is to be raised above reservoir)
- Determine friction loss (losses due to piping depend on size, length and condition of piping system in relation to G.P.M. needed, see table below. Friction losses also include loss due to valves and fittings)
- 3. Determine velocity head (refer to table below) $V_{H} = \left(\frac{Vel}{8.02}\right)^2$
- 4. Total all three of the above and compare to performance chart. Select pump which delivers total head at desired G.P.M.
 DIPE EDICTION
 Loss of Head in Feet, Per 100 Ft, of 15-year-old Ordinary

Gallens	16"	Fipe .	- 14"	Pipe	1"1	lipe	1%*	Pipe	1%"	Pipe	2" 1	lpe	2%"	Fipe	3" P	ipe
Minute	Vel.	Fric.	Vel.	Fric.	Vel.	Fric.	Vel.	Fric.	Vel.	Fric.	Vel.	Fric.	Vel.	Fric.	Vel.	Fric.
1	1.05	2.1				1.1.1										
2	2.10	7.4	1.20	1.9		-						-			and a	
3	3.16	15.8	1.80	4.1	1.12	1.26										
4	4.21	27.0	2.41	7.0	1.49	2.14	0.86	0.57	0.63	0.26			1.1			· · · · ·
5	5.26	41.0	3.01	10.5	1.86	3.25	1.07	0.84	0.79	0.39						
10	10.52	147.0	6.02	38.0	3.72	11.7	2.14	2.05	1.57	1.43	1.02	0.5	0.65	0.17	0.45	0.07
15			9.02	80.0	5.60	25.0	3.2	6.5	2.36	3.0	1.53	1.0	0.98	0.36	0.68	0.15
20			12.03	136.0	7.44	42.0	4.29	11.1				1.83	1.31	0.61	0.91	0.25
25					9.30	64.9	5.36	16.6	3.94	7.8	2.55	2.73	1.63	0.92	1.13	0.38
30					11.15	89.0	6.43	23.5	4.72	11.0	3.06	3.84	1.96	1.29	1.36	0.54
35				·	13.02	119.0	7.51	31.2	5.51	14.7	3.57	5.1	2.20	1.72	1.59	0,71
40	1.11				14.88	152.0	8.58	40.0	6.3	18.8	4.08	6.6	2.61	2.20	1.82	0.91
45					1		9.65	50.	7.08	23.2	4.60	8.2	2.94	2.80	2.05	1,15
50							10.72	60.	7.87	28.4	5.11	9,9	3.27	3.32	2.27	1.38
70							15.01	113.	11.02	\$3.0	7.15	18.4	4.58	6.2	3.18	2.57
90									14.17	84.0	9.19	29.4	5.88	9.8	4.09	4.08
100									15.74	102.0	10.21	35.8	6.54	12.0	4.54	4.96
120									18.89	143.0	12.25	50,0	7.84	16.8	5.45	7.0
140		1000							22.04	190.0	14,30	67.0	9.15	22.3	6.35	9.2
160			100000			ation of					16.34	86.0	10.46	29.0	7.26	11.8
180	A state					. And And					18.38	107.0	11.76	35.7	8.17	14.8
200											20.42	129.0	13.07	43.1	9.08	17.8
220	1.5.										22.47	154.0	14.38	52.0	9.99	21.3
240					1.11						24.51	182.0	15.69	61.0	10.89	25.1
260											26.55	211.0	16.99	70.0	11.80	29.1
280													18.30	81.0	12.71	33.4
300					1.1.1					(and		inter	19.61	92.0	13.62	38.0

Friction of Water in 90° Elbows

Size of Elbow, Inches	34	- 45	T.	1%	1 16	1	2%	3	4	3	6
Frittion Equivalent Foot Streight Pipe	5	4					11	15	14	18	18

To Compute Break Horse Power

BHP = GPM x H x S.G. 3960 x pump Eff.* S.G. = Specific Gravity, BHP = Break Horse Power, GPM = Gallons per Minute, H = Head in Feet Eff. = Efficiency

Horse Power and Pressure (PSI) vary in direct proportion to the Specific Gravity.

Effect of Speed Changes

- Capacity (GPM) is directly proportional to the change in speed.
- Head is proportional to the square of the change in speed.
- Horse Power is proportional to the cube of the change in speed.

Pipe Friction (Continued)

Loss of Head in Feet, Per 100 Ft. of 15-year-old Ordinary Iron Pipe Due to Friction.

Guillere	4"	Fipe .	8"	Pige .	6"	fipe
Minute	Vel.	Pris.	Vel.	Feic.	Vel.	Fric.
40	1.02	0.22	1000			
45	1.17	0.28	1000	1.000	1114	10.00
. 50	1.28	0.34	1.12	0.75	- 1114 ·	10.00
70	1.02	0.43	1.22	0.24		
100	2.44	1.71	1.63	0.19	1.14	0.14
135	3.04	121	1.96	0.57	1.47	0.75
125	3.19	1.66	2.04	0.64	1.48	0.28
1.50	3.84	2.55	2.45	0.88	1.71	0.33
175	4.45	3.36	2.85	1.18	2.00	0,41
200	5.11	4.37	3.27	1.48	2.28	0.63
228	6.32	6.61	3.67	1.86	2.57	0.74
250	6.40	8.72	4.08	2.34	2.80	0.7
200	7.44	9.18	4.90	3.15	3.40	1.2
350	8.90	19.32	5.72	4.19	3.56	1.4
400	10.70	15.82	6.54	5.33	4.54	2.2
450	11.50	19.74	7.35	6.65	5.12	2.7
475	12.30	22.96	7.88	7.92	8.55	3.2
\$00	12,77	24.08	8,17	8,12	5.60	3.3
550	1000		9.09	9.46	6.16	1.9
600	1000	4	9.80	11.34	6.72	1.1.1
705			11.44	15.12	7.84	A 1
7.50		2000	12.36	17.32	8.50	7.0
800					9.08	7.9
850					9.58	8.7
900		+++++			10.20	10,1
1000	++++	1. +		++++	10.72	12.0
1100	++++			++++	13.40	14.5
1200				1100	13.53	16.0

THEORETICAL DISCHARGE OF NOZZLES IN U.S. GALLONS PER MINUTE

HEA	Ð	Velocity of	-	11.5		DIAMETER	OF NOZZLE	IN INCHES			
Pounds	Feet	Discharge Feel Per Second	¥14	%	¥10	14	%	%	%	34	7/8
10	23.1	38.6	0.37	1.48	3.32	5.91	13.3	23.6	36.9	53.1	72.4
15	34.6	47.25	0.45	1.84	4.06	7.24	16.3	28.9	45.2	65.0	88.5
20	46.2	54.55	0.52	2.09	4.69	8.35	18,8	33.4	52.2	75.1	102
25	57.7	61.0	0.58	2.34	5.25	9.34	21.0	37.3	58.3	84.0	114
30	69.3	65.85	0.64	2.50	5.75	10,2	23.0	40,9	03.9	92.0	120
35	80.8	72.2	0.69	2.77	6.21	11.1	24.8	44.2	69.0	99.5	135
40	92.4	77.2	0.74	2.96	6.64	11.8	26.6	47.3	73.8	105	145
45	103.9	81.8	0.78	3.13	7.03	12.5	28.2	50.1	78.2	113	153
50	115.5	86.25	0.83	3.30	7.41	13.2	29.7	52.8	82.5	119	162
55	127.0	90.4	0.87	3,46	7.77	13.8	31.1	55.3	86.4	125	169
60	138.6	94.5	0.90	3.62	8.12	14.5	32.5	57.8	90.4	130	177
65	150.1	98.3	0.94	3.77	8.45	15.1	33.8	60.2	94.0	136	184
70	161.7	102.1	0.96	3.91	8.78	15.7	35.2	62.5	97.7	141	191
75	173.2	105.7	1.01	4.05	9.08	16.2	36.4	64.7	101	146	198
80	184.8	109,1	1.05	4.18	9.39	16.7	37.6	66.8	104	150	205
85	198.3	112.5	1.08	4.31	9.67	17.3	38.8	68.9	108	155	211
90	207.9	115.8	1.11	4.43	9,95	17.7	39.9	70.8	111	160	217
95	219.4	119.0	1.14	4.56	10.2	18.2	41.0	72.8	114	164	223
100	230.9	122.0	1.17	4.67	10.0	18.7	42.1	74.7	117	168	229
105	242.4	125.0	1.20	4,79	10.8	19.2	43.1	76.5	120	172	234
110	064.0	109.0	1.00	4.00	11.0	10.6	44.1	78.4	122	176	240
110	204.0	120.0	1.05	5.01	11.0	20.0	45.1	80.1	125	180	245
100	200.5	130.9	1.00	5.10	11.5	20.5	46.0	81.8	128	184	251
120	277.1	133.7	1.20	5.99	11.7	20.0	47.0	83.5	130	168	256
125	258.5	130.4	1.21	5.22	12.0	21.3	48.0	85.2	133	192	261
130	300.2	139,1	1,00	0.00	12.0	E1.5	40.0	68.2	150	105	300
135	311.7	141.8	1.38	5.43	12.2	21.7	46.9	00.7	130	190	271
140	323.3	144.3	1.38	5.53	12.4	22.1	49.8	88.4	130	202	975
145	334.8	146.9	1.41	5.62	12.6	22.5	50.6	89.9	140	202	210
150	346.4	149.5	1.43	5.72	12.9	22.9	51,5	91.5	143	200	200
175	404.1	161.4	1.55	6.18	13.9	24./	50.0	106	105	238	302
200	461.9	172.6	1.65	6.61	14.8	26.4	59.5	100	100	230	ded.
HE	AD	Velocity of				DIAMETER	R OF NOZZLE	E IN INCHES			
Pounds	Feet	Feet Per Second	1	1%	1%	13%	11/2	13%	2	21/4	21/3
10	23.1	38.6	94.5	120	148	179	213	289	378	479	591
15	34.6	47.25	116	147	181	219	260	354	463	585	72
20	46.2	54.55	134	169	209	253	301	409	535	676	83
25	57.7	61.0	149	189	234	283	336	458	598	756	93
30	69.3	66.85	164	207	256	309	368	501	655	828	102
9.6	80.8	20.0	177	024	977	994	398	641	708	895	110
40	00.8	77.0	100	230	204	357	426	578	756	957	118
40	102.9	111.0	200	263	313	379	451	613	801	1015	125
-0	115.5	86.95	211	267	330	399	475	647	845	1070	132
66	197.0	00.0	201	280	345	418	498	678	886	1121	136
00	127.0	00.0	0.01	200	0.00	400	504	700	000	1170	1.14
60	138.6	94.5	231	293	362	438	521	708	920	1000	164
65	150.1	98.3	241	305	376	455	542	737	304	1260	150
70	161.7	102.1	250	317	391	4/3	563	765	1001	1207	100
75	173.2	105.7	259	327	404	489	582	782	1037	1310	101
80	184.8	109.1	267	338	418	505	602	818	1010	1354	107
85	196.3	112.5	276	349	431	521	620	844	1103	1395	172
90	207.9	115.8	284	359	443	536	638	868	1136	1435	177
95	219.4	119.0	292	369	456	551	656	892	1168	1476	182
100	230.9	122.0	299	378	467	565	672	915	1196	1512	187
105	242.2	125.0	306	388	479	579	689	937	1226	1550	191
110	254.0	128.0	314	397	490	593	705	960	1255	1588	196
115	265.5	130.9	320	406	501	606	720	980	1282	1621	200
120	277 4	133.7	327	414	512	619	736	1002	1310	1639	205
125	288.6	136.4	334	423	522	632	751	1022	1338	1690	209
130	200.0	130.1	541	493	593	645	767	1043	1365	1726	213
130	000.2	130.1	041	100	500	000	700	1000	1000	1750	247
135	311.7	141.8	347	439	543	600	780	1063	1390	1700	201
		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	1.46.4	448	553	666	785	1062	1410	1/80	221
140	323.3	144.3	004		1000	0.000	800	1 1 1 1 1 1	1 4 6 6	1000	0.00
140 145	323.3 334.8	146.9	360	455	562	680	809	1100	1400	1820	225
140 145 150	323.3 334.8 346.4	144.3 146.9 149.5	360 366	455 463	562 572	680 692	809 824	1100	1400	1820	225
140 145 150 175	323.3 334.8 346.4 404.1	144.3 146.9 149.5 161.4	360 366 395	455 463 500	562 572 618	680 692 747	809 824 890	1100 1120 1210	1400 1466 1582	1820 1853 2000	225 229 247

NOTE-The actual quantities will vary from these figures, the amount of variation depending upon the shape of nozzle and size of pipe at the point where the pressure is determined. With amount taper nozzles the actual discharge is about 94 per cent of the figures given in the labels.

MAINTENANCE HISTORY

MODEL NO.	IMP	DIA.	
OPERATING COND.	GPM @	FT. THD	
HP	SPEED/RI	PM	
Start-Up Date	Amps a	t Start-Up	
Pressure at Start-Up			

ENGINEERING DATA

POWER FRAME	52HD	53HD	54HD
1. RADIAL BRG.	41211	41316	41319
2. THRUST BRG.	41308-DR	41312-DR	41314-DR
3. BALL BRG, SPAN	9.032	12.750	12.750
4. SHAFT DIA'S.			
@ RADIAL BRG.	2.1655	3.1497	3.7403
@ THRUST BRG.	1.5750	2.3623	2.7560
@ THROTTLE BUSHING	1.735	1.875*	2.500
@ IMPELLER	1.375	1.500	1.750
BET BALL BRG'S.	1.937	3.125	3.625
BET RADIAL BRG.	The second s	24.53	
& THROTTLE SLV.	2.250	3.250	4.250
	1000	*2 010 (6x6-14	1

GREASE LUBRICATION

DATE	GREASED	DATE	GREASED	DATE	GREASED
1.15		1000			
			the second second		

TYPE GREASE USED.

COUPLING ALIGNMENT

Parallel Alignment					Angular Alignment						
Date Checked	Amt. Out	Date Checked	Amt. Out	Date Checked	Amt. Out	Date Checked	Amt. Out	Date Checked	Amt. Out	Date Checked	Amt. Out
	-	-	-	-	-	-	-	-	-		-
	-		-								
NOTES:											

Product Profile

SEVERE DUTY CENTRIFUGAL SEPARATOR

MODEL # SDS SERIES SEPARATOR

PRODUCT FEATURES

THE EBBCO SDS CENTRIFUGAL SEPARATORS ARE DESIGNED TO REMOVE SOLIDS FROM LIQUIDS. EACH MODEL IS SIZED BASED UPON THE FLOW RATE.

UPON TANGENTIAL ENTRY, THE LIQUID AND SOLIDS ARE DRAWN THROUGH INTERNAL SLOTS AND ACCELERATE INTO THE SEPARATION CHAMBER. SOLIDS THAT ARE HEAVIER THAN THE CARRYING LIQUID ARE SEPARATED AND ACCUMULATED IN THE COLLECTION CHAMBER. THE SOLIDS ARE PERIODICALLY PURGED INTO A COLLECTION VESSEL. CLEAN LIQUID IS DRAWN UP AND OUT OF THE SEPARATOR

- NO MOVING PARTS TO WEAR OUT.
- LOW PRESSURE LOSS.
- NO BACKFLUSHING.
- NO DOWNTIME REQUIREMENTS.
- NO SCREENS, CARTRIDGES, CONES, OR FILTER ELEMENTS TO CLEAN OR REPLACE.
- FLOW RATES FROM 45-1200 GPM

PROVEN APPLICATIONS

- ABRASIVE WATERJET-GARNET REMOVAL.
- PARTS WASHERS.
- HEAT TREATMENT SYSTEMS.
- MACHINE TOOL COOLANT FILTRATION.







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Specifications

SEVERE DUTY CENTRIFUGAL SEPARATOR

MODEL # SDS SERIES SEPARATOR

MAX PRESSURE PRESSURE LOSS RANGE FLOW RANGE MAX PARTICLE SIZE MATL OF CON. 150 psi 5-12 psi 45-1200 gpm 3/8" CARBON STEEL (STAINLESS STEEL OPTIONAL)

*CONSULT FACTORY FOR HIGHER FLOW RATES AND OPERATING PRESSURES

<u>CAUTION:</u> FOR USE WITH A CENTRIFUGAL PUMP ONLY! DO NOT USE WITH A POSITIVE DISPLACEMENT PUMP.



MODEL	Α	В	С	D	E	FLOW	INLET/	PURGE	WEIGHT	WEIGHT
						RANGE	OUTLET	SIZE	DRY	WET
0150-B	30	4 ³ / ₈	4 ³ / ₄	1¾	6	45-70	1 1/2"	1 1/2"	27	40
0200-B	335∕8	5	51⁄2	25⁄8	85⁄8	65-108	2"	1 1/2"	52	98
0250-B	37	51⁄2	6¼	25⁄8	85⁄8	98-155	2 1/2"	1 1/2"	60	109
0300-B	42	7	81⁄4	3¼	10¾	148-290	3"	1 1/2"	101	177
0400-B	88	141⁄2	10	3 1⁄8	11	275-550	4"	1 1/2"	300	410
0500-B	108	16¼	12	3 11/16	11	480-880	6"	1 1/2"	415	615
0600-B	108	16¼	12	3 11/16	11	720-1200	6"	1 1/2"	475	714

ALL DIMENSION (") ALL FLOW IN (USGPM)

Product Profile

TANK EDUCTORS

TO KEEP UNWANTED SOLIDS FROM SETTLING IN A SUMP, EBBCO EDUCTORS PROVIDE A VENTURI ACTION, WHICH AMPLIFIES THE INPUT FLOW RATE TO SWEEP SOLIDS TOWARDS THE PUMP INTAKE.

- HELPS TO AVOID TROUBLESOME ACCUMULATION
- REDUCES MAINTENANCE AND SHUTDOWN ROUTINES
- PROTECTS PUMPS AND PROCESS FLUID SYSTEMS FROM FOULING AND/OR ABRASIVE WEAR FROM UNWANTED SOLIDS
- MINIMIZES BACTERIAL GROWTH, BROUGHT ON OTHERWISE BY SOLIDS ACCUMULATION
- LIMITS THE NEED FOR CHEMICAL TREATMENTS TO CONTROL BACTERIAL & ALGAE BT PREVENTING SOLIDS BUILD UP

ABLE TO OPERATE AT LOW PRESSURES AND IN LOW SUBMERGANCE. EBBCO EDUCTORS MULTIPLY THE FLOW RATE BY A FACTOR OF FOUR OR FIVE ENABLING THE USE OF A SMALLER PUMP TO REDUCE ENERGY COSTS. COMPACT IN DESIGN, DURABLE AND EASY TO INSTALL.

MALT OF CONST. PDVF (KYNAR), 316 SS, GLASS FILLED PP, CAST IRON

MODEL	10	15	20	25	30	35	40
No			NOZZL	E FLOW	(US GPI	M)	
0MP	7.5	9.2	10.7	11.9	13.1	14.1	15
2MP	13.5	17	19	21	23	25	27









<u>2MP</u>





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Product Profile

Abrasive Bag Hopper

MODEL # GRS-ABH



Description:

•

The Ebbco one cu.yd. Abrasive Bag Hopper is designed to capture up to 4000 lb. of garnet. Spent garnet that is discharge from the centrifugal separator is collected into the Abrasive Bag Hopper. The heavy garnet settles to the bottom of the Abrasive Bag Hopper and begins to de-water itself. The excess fluid that is purged into the Abrasive Bag Hopper flows out of the collection bag and decants back to the catch tank. The Abrasive Bag Hopper is constructed from 1/4" carbon steel plate.

- Dimensions: 36"L x 36"W x 48"H
- Material of cont.: Carbon Steel
 - Finish: Industrial enamel paint
- Dry Weight 580 lb.

System Features & Benefits:

- Clean and easy system for handling spent abrasive.
- Spent abrasive is bagged and ready for recycling or reclamation.
- Rouged construction.
- Clean out ports.
- Fork truck access.



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Ebbcoinc. METALWORKING FILTRATION & FLUIDS

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	I			_
RN REF	PART #	VENDOR	NOTE	-
		EBBCO		7
		EBBCO		-
		EBBCO		7
		EBBCO	EF-1.50-TE-P8-SS	
		EBBCO EBBCO	OMP EF-1.00-0.375-RB-P8-TT	F
		EBBCO	EF-1.50-1.00-RB-P8-ST	
		EBBCO EBBCO	EBF-1.00-NO-P8 EF-1.00-0.375-RB-P8-S1	-
		EBBCO	EF-1.00-E4-P8-SS	
		EBBCO EBBCO		-
		EBBCO		
	EF-3.00-2.50-RB-CI-	EBBCO TT EBBCO		-
		EBBCO		
F ITE A B C D	PVC PIPE 0 EM QTY 1 1 8 5	CUT LIST LENG 72" 84" 16" 20"		
ES: SSEMBL HTEN. (LOW. PI	E THREADED FITTING CLEAN AND GLUE SLI PE DOPE, CLEANER, /	35 WITH PIPE DOP P FITTINGS AS DE: AND CEMENT ARE	E AND SCRIBED INCLUDED.	с
ES: SSEMBL GHTEN, G LOW, PI DRTANT RRECT G	E THREADED FITTING CLEAN AND GLUE SLI PE DOPE, CLEANER, / 	SS WITH PIPE DOP P FITTINGS AS DE AND CEMENT ARE	E AND SCRIBED INCLUDED.	С
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1.	System is positioned properly.							
2.	Sweeper package has been installed ac	Sweeper package has been installed according to drawing provided by Ebbco.						
3.	All external connections have been made between Garnet Removal System and waterjet catch tank; and proper air supply has been hooked up to plant air minimum 80 PSI @ 2 SCFM.							
4.	System runs with a 4 to 10 PSI pressure	System runs with a 4 to 10 PSI pressure differential between inlet and outlet of separator.*						
5.	Good water movement in waterjet catcher tank.							
6.	System runs with no leaks.							
7.	Purge is set for a four (4) second purge every 60 seconds; water should flow back from the Garnet Hopper to the waterjet cutting tank.*							
8.	Customer understands how system works and how to service the strainer basket.							
9.	Customer knows how, and when, to empty spent Garnet Hopper.*							
10.	Overflow baffle is installed in Garnet Hop	oper.*						
11.	Use only Ebbco certified consumables a failure.	nd replaceme	nt parts. Fai	lure to do so may cause catastrophic				
12.	System is designed to run simultaneousl cut.	y with waterje	t. Always rur	n your Garnet Removal System while you				
*Note: Iter Failure to fe performand I have read be adhered	tem numbers 4, 7, 9, and 10 must be follow follow above instructions can lead to catas nce. The Garnet Removal System has been ad and understand the Ebbco Service Manu- ed to.	trophic failure installed and ial. I agree th ATING PRESS	intained or v of the Ebbcc is operating at proper sys	varranty is null and void. Garnet Removal System as well as poor correctly according to the service manual. tem maintenance and filter change out will				
	IIIIer	Outlet	Vac					

FOLLOW PROPER LOCKOUT PROCEDURE BEFORE SERVICING THIS EQUIPMENT.

GARNET REMOVAL INSTALLATION REGISTRATION AND ACCEPTANCE FORM

Ebbco Technician <i>(if on site)</i>	Company
Supervisor	Contact Name
Operator	Contact Phone Number
Operator	Contact E-Mail Address
INSTALL DATE:	SERIAL NO:

NOTE: Warranty on equipment is null and void if this form is not completed and returned to Ebbco upon installation. Email to: customerservice@ahbinc.com

DANGER